

Response surface methodology guided approach for optimization of protein isolate from Faba bean. Part 1/2

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1 Response surface methodology guided approach for optimization of protein isolate from

Faba bean. Part 1/2

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11 ABSTRACT

Ultrasound-assisted extraction (UAE) was evaluated as a green procedure to produce faba 12 beans protein isolates from faba beans. Magnetic stirring was performed as conventional 13 extraction. A three-level five-factor Box-Behnken Design (BBD) was applied to obtain the 14 15 optimal UAE conditions to concurrently maximize extraction yield and protein content. The response surface methodology (RSM) showed a quadratic curvature for extraction yield and 16 protein. The optimal extraction conditions were determined as: Power of 123 W, solute/solvent 17 18 ratio of 0.06 (1:15 g/mL), sonication time of 41 min, and total volume of 623 mL with a desirability value of 0.82. Under these conditions, the extraction yield of 19. 75 \pm 0.87 % 19 (Protein yield of 67.84%) and protein content of 92.87 ± 0.53 % were obtained for optimum 20 ultrasound extraction. Control samples using magnetic stirring under similar conditions 21 22 without ultrasound treatment showed an extraction yield of 16.41 ± 0.02 % (Protein yield of 54.65 %) and a protein content of 89. 88 ± 0.40 %. This shows that BBD can effectively be 23

used to optimize the extraction of proteins from faba beans using optimal extraction conditions,

resulting in a higher extraction yield and protein purity.

26 Keywords: Faba beans, Ultrasound extraction, response surface methodology, Box-Behnken

27 Design, Process optimization, Protein isolate

28

29 INTRODUCTION

Expected demand for conventional proteins from animals, seafood and dairy sources is 30 31 projected to increase by 2050 globally mostly for animal proteins (Hayes, 2023). Additional 32 animal farming is linked to higher emissions of greenhouse gases (Manzano et al., 2023), increasing land and water use, along with growing concerns about risk of health issues related 33 to red meat intake, as well as ethical and religious disagreements tied to the slaughter of animals 34 35 by certain sectors of the population (Pam Ismail et al., 2020). These growing concerns and issues have driven researchers within the food industry to explore alternative environmentally 36 friendly and renewable sources of proteins to curb these problems (Surya Ulhas et al., 2023). 37 Thus, there has been a transition towards the search for alternatives, which generally includes 38 39 proteins from aquatic sources (duckweed, microalgae, and macroalgae), bacterial and fungal sources, and plants-based sources (pulse, legume, oilseed, cereal, and food- byproducts) 40 (Badjona et al., 2023c; Fasolin et al., 2019). In comparison to conventional sources, these 41 alternative protein sources have several benefits, such as lower greenhouse gas emissions and 42 carbon footprint during production, low production costs, efficient resource utilisation, and 43 increased acceptance by consumer as the nutritional trends of individuals such as flexitarianism 44 is on the rise (Badjona et al., 2023a; Takefuji, 2021). 45

46 Faba beans are a cool seasonal legume that is widely cultivated in Australia, Egypt, Ethiopia,

47 Germany, Canada, and the United Kingdom. While this legume has a high protein content, ease

of cultivation, and superior nitrogen-fixing capabilities; large amounts of faba bean ingredients 48 are not employed in food systems (Khazaei et al., 2021). Whole faba beans contain 20–35% 49 protein, 1–2% fat, 55–65% carbohydrate, 10–15% fiber, and vitamins and minerals such as 50 51 iron, zinc, calcium, potassium, and magnesium. The presence of phytochemicals in faba beans has been suggested to provide numerous health benefits (Badjona et al., 2023b). According to 52 53 their sedimentation coefficient, globulins, which make up 70-80 % of the storage protein in faba beans, may be divided into two classes: the 7S vicilin-type globulins and the 11S legumin-54 type globulins (Fiel et al., 2002). Extraction of proteins from this sustainable and renewable 55 legume is worth considering for specialized applications in food systems such as emulsions 56 57 (Dubey et al., 2016; Paximada et al., 2021).

Extraction of proteins from plant materials by alkaline-isoelectric precipitation generally 58 involves solubilisation of the aqueous systems in alkaline condition followed by precipitation 59 60 of the proteins at their isoelectric point for food applications. Unfortunately, this approach only extracts roughly half of the proteins, with the remaining lost to discarded solids and liquids 61 (Chandran et al., 2023; Hewage et al., 2022). Lower extractability may be attributed to inherent 62 63 protein-carbohydrate complexes present in certain locations of the raw material (Eze et al., 64 2022a). Hence, to improve the extraction yield of proteins, advanced and novel technologies such as ultrasound-assisted extraction, ohmic heating, microwave extraction supercritical fluid 65 extraction and pulsed electrical field application have been promoted (Eze et al., 2022b). 66 67 Ultrasound processing is regarded as an eco-friendly, non-toxic, relatively cheaper and timeefficient technique that can be employed to improve extraction yield (Suchintita Das et al., 68 2022a). The effect of ultrasound can be ascribed to cavitational effects which aid in the 69 disruption and disintegration of cellular matrices and the subsequent release of proteins. 70

Thus, this present study aims to examine the efficiency of ultrasound-assisted protein extraction
from faba beans by varying key processing factors such as sonication power, treatment time,

solute-to-solvent ratio, and total extraction volume through the application of response surface
methodology (RSM). RSM studies may also differ in the response variable. In this study, the
response variable was optimized for extraction yield and protein content.

76 MATERIALS AND METHOD

77 Raw Materials and Chemicals

Faba bean seeds was obtained from Whole Foods Earth (Kent, United). NaOH, (\geq 99.9 %

79 pure), and HCI was also obtained from Sigma-Aldrich (United Kingdom). The seeds were

80 milled using a cyclone mill.

81 Ultrasound-assisted alkaline extraction (UAE) of protein isolates from faba beans

Different dispersions of faba bean flour in water (1:5 - 1:20 w/v) with variable total volumes 82 83 (500 – 1000 mL) were agitated at 25 °C for 20 minutes at 500 rpm prior to ultrasonic-assisted extraction. The dispersion was then adjusted to pH 11 using 1M NaOH, then subjected to 84 85 ultrasonic treatment at varying ultrasonic power (50 - 180 W) and varying sonication duration (10 - 60 min) based on a previous study (Badjona et al., 2024a) using a S24d22D titanium 86 ultrasonic horn (Teltow, Germany). Temperature was maintained at 20 - 25 °C using an ice bath. 87 The resultant mixture was centrifuged for 20 minutes at 25 °C at 6,000 rpm (accuSpinTM 400, 88 United Kingdom). After gathering the supernatant, 1 N HCI was used to bring the pH to 4.0 89 90 while stirring continuously for 20 minutes. Protein isolate pellets were then obtained after centrifuging at 6,000 rpm for 20 min at 25°C. After 48 hrs of lyophilization of the protein pellet, 91 samples were stored at -20 °C for further analysis. Protein content was determined by the 92 Dumas method using a nitrogen conversion factor of 6.25. Control protein isolate was 93 generated using optimized conditions without ultrasound treatment. 94

- 95 The weight of the protein isolate obtained was divided by the initial weight of the measured
- 96 faba bean flour to calculate the extraction yield, as given in Equation (1).

97 Extraction yield (%) = $\frac{m_p \times 100}{m_i}$ (Eq.1)

98 The mass of the initial flour and final protein isolate is represented by *mi* and *mp*, respectively.



Fig.1. Schematic diagram of ultrasound-assisted extraction of faba bean protein isolate (NB:
(a) screen values (b) ultrasound control system (c) Converter (d) probe horn (e) flour
suspension (f) magnetic stirrer.

102 Experimental design and optimization

The Box-Behnken design was implemented to establish the optimal conditions for ultrasound-103 assisted extraction of proteins from faba beans. The response surface-based optimization 104 method was carried out using Design Expert software to obtain the maximum extraction yield 105 and protein content from faba bean flour. The extraction variables consisted of three distinct 106 levels for each of the four variables. The solid/solvent ratio (g/mL) (X1), total volume (mL) 107 (X_2) , ultrasound power (W) (X_3) , and extraction time (min) (X_4) were the independent variables 108 109 for the ultrasonic-assisted alkaline extraction of fava bean protein isolates that were investigated at three different levels of low (1), medium (0) and high (+1). Both the extraction 110 yield and protein content of the freeze-dried faba bean protein isolate were used as the response 111 variables. The coded factors for each variable are displayed in Table 1. 112

113	Table 1. Actual and coded variables were used in the ultrasound-assisted extraction design of
114	the experiment.

Independent	Unit		Levels	Levels		
Variables		Low	optimal	High		
Power	W	50	115	180		
Solute/water ratio	w/v	0.06	0.15	0.25		
Extraction time	min	10	35	60		
Total volume	ml	500	750	1000		

The experimental data were evaluated with the goal of identifying the optimal set of parameters 116 that would produce the highest extraction yield and protein content values to identify the major 117 influencing factors. The results of our earlier research (Badjona et al., 2024a) and those of other 118 authors who obtained protein isolate from plant sources were used to determine the minimum 119 and maximum amounts assigned to each factor (Alvarez-Ossorio et al., 2022; Fatima et al., 120 2023). Actual and coded variables employed in the UAE experimental design are shown were 121 used. The second-order polynomial model was obtained by data analysis of the response and 122 independent variables. 123

124
$$EY(\%) = \beta_0 + \beta_1 X_1 + \beta_2 X_1^2 + \beta_3 X_2 + \beta_4 X_2^2 + \beta_5 X_3 + \beta_6 X_3^2 + \beta_7 X^4 + \beta_8 X_4^2$$

 $125 \qquad + \ \beta_9 X_1 X_2 + \beta_{10} X_1 X^3 + \beta_{11} X_1 X_4 + \beta_{12} X_2 X_3 + \beta_{13} X_2 X_4 + \beta_{14} X_3 X_4 \ (\text{Eq.2})$

- where X_i and X_j are independent variables; β_0 is the intercept; β_i , β_{ii} , and β_{ij} are the
- 127 coefficients of the linear, quadratic, and interaction term, respectively; and EY is the response
- 128 variable, which includes the protein content and extraction yield.

129 RESULTS AND DISCUSSION

130 Fitting response surface models

The process of extraction has a significant impact on the functional attribute of any given 131 protein. As a result, choosing and verifying the best extraction technique requires a thorough 132 examination. Since the current conventional procedures have numerous drawbacks, novel 133 enhanced extraction techniques have been suggested as an alternative (Suchintita Das et al., 134 2022b). To achieve maximal response in terms of extraction yield and protein content 135 simultaneously in UAE, variables such as Power (A), Solute-to-solute ratio (B), Sonication 136 time (C), and Total volume (D) optimization were carried out using a statistical response 137 surface model. A total of 29 runs were carried out utilizing the BBD to evaluate and optimize 138 the combined influence of the four process parameters on both response variables. The 139 methodology for fitting models is a significant advancement over earlier approaches because 140 it makes explicit assumptions that might otherwise remain hidden, makes the most use of the 141 information contained in a set of data, and provides a "goodness-of-fit test" to determine 142 whether a model is significant prior to analysis (Boateng et al., 2023). As observed in Table 2, 143 the extraction yield ranged from 15.23 to 19.13 %. The highest yield value (19.13 % was 144 achieved at a solute-to-solvent ratio of 0.06 (1:15 g/mL), sonication power of 180 W, total 145 extraction volume of 750 mL, and 35 min of ultrasound treatment. 146

147

150 Table 2. Predicted and experimental values from the Box-Behnken design matrix

	Fact	Factor	Factor 3	Factor 4	Response 1		Response 2	
	or 1	2						
Run	Δ.	B∙	C.	D: Total	Extraction	Predicted	Protein	Predicted
ixuii	- T .	D.	C.	D. Total		Treateted	Tiotem	Treateted
	Pow	Solute/	Sonication	volume	yield (g/100g)		content %	
	er	water	time		Experimental		Experimental	
	W	S/W	min	ml	%			
6	115	0.155	35	750	17.85	17.56	92.86	91.20
15	115	0.155	35	750	17.89	17.56	91.94	91.20
24	115	0.06	35	1000	16.61	16.69	91.69	89.04
17	50	0.06	35	750	16.59	16.06	91.19	92.52
14	180	0.155	10	750	16.96	17.58	90.56	86.39
25	115	0.155	35	750	17.36	17.56	90.50	91.20
28	115	0.155	35	750	17.36	17.56	90.38	91.20
27	115	0.155	35	750	17.35	17.56	90.30	91.20
2	115	0.25	35	1000	17.01	17.45	90.06	84.74
29	115	0.06	35	500	18.52	18.66	90.00	89.11
12	50	0.155	35	1000	15.23	15.23	89.94	89.91
26	50	0.155	10	750	15.27	15.72	89.50	87.16

9	50	0.155	60	750	16.39	16.35	89.31	87.28
4	180	0.155	60	750	18.04	18.04	88.75	84.89
13	115	0.06	60	750	18.11	18.63	87.88	88.18
23	115	0.06	10	750	16.82	16.99	87.00	87.62
16	115	0.155	10	500	17.94	17.68	86.81	87.33
5	115	0.25	35	500	17.32	17.32	86.5	82.94
3	50	0.155	35	500	16.54	16.54	86.13	86.89
22	180	0.155	35	500	18.52	18.24	84.81	87.46
1	180	0.06	35	750	19.13	18.74	84.63	85.91
7	115	0.155	60	1000	17.15	17.12	84.44	87.51
10	180	0.155	35	1000	17.56	17.24	84.31	86.17
8	115	0.155	60	500	18.08	17.95	83.88	84.39
20	180	0.25	35	750	17.64	17.87	83.45	85.70
18	115	0.155	10	1000	16.34	16.17	82.88	85.94
19	115	0.25	10	750	18.79	17.98	81.31	83.63
11	50	0.25	35	750	16.77	16.86	79.94	82.25
21	115	0.25	60	750	18.01	17.56	79.69	81.69

As shown in **Table 3**, analysis of variance (ANOVA) was used to evaluate the proposed model 154 equation. A lower p-value (p < 0.0001) for extraction yield demonstrated that the fitted models 155 were significant. The F-values and p-values of lack-of-fit models implied that it was not 156 significantly relative to the pure error indicating the suitability of the model for optimization 157 (Sahu et al., 2020). For the quadratic regression models, the calculated correlation coefficient 158 (\mathbf{R}^2) was 0.83 indicating that 83 % of the variances could be explained by the fitted model (Fig 159 2). In this experiment, A, C, D, BC, and A² were significant model items while the other terms 160 were insignificant (p > 0.05). With regards to protein content, the developed model showed a 161 p-value of 0.20 indicating that the model was not significant. 162

The computed correlation coefficients (R^2) for protein content in the quadratic regression 163 model were 0.61, meaning that 61% of the variations could be accounted for by the fitted 164 model. In this case, B, B², and C² were the only significant model terms with regard to protein 165 166 content. The reason for the insignificance in protein content could be due to the use of constant solubilization pH and precipitation pH. In this study, there was no need to optimize the pH as 167 the precipitation pH of proteins from legumes is well documented (Jeganathan et al., 2023; 168 169 Langton et al., 2020). Herein, the experimental dataset was subjected to a regression analysis 170 to fit in the established second-order quadratic model. Regression analysis was performed on this experimental dataset to attempt to fit it into the established second-order quadratic model. 171 The following polynomial equation expresses the predicted extraction yield and protein 172 173 content.

174	Extraction yield (%) = 17.562 + 0.92A - 0.02B + 0.305C - 0.585D - 0.4175AB -0.01AC +
175	$0.0875AD - 0.5175BC + 0.4BD + 0.1675CD - 0.51A^2 + 0.33B^2 - 0.099C^2 + 0.234D^2$

176Protein content (%) = 91.1975 - 0.790625A - 2.619166667B - 0.343541667C + 0.4325D +1772.5175AB - 0.40625AC - 1.078125AD - 0.625BC + 0.46875BD + 1.124375CD -178 $1.726979167A^2 - 2.875416667B^2 - 3.042604167C^2 - 1.862916667D^2$

179 where A, B, C, and D are the independent variables for Power (A), Solute-to-solvent ratio

180 (B), Sonication time (C), and Total volume (D), respectively.



184 Fig 2. Regression coefficient of quadratic model for extraction yield (%) and protein content185 (%).

	192	Table 3. Va	ariance analys	is for the protein	content and extraction	on yield (%)	regression model.
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Source	Extraction yield (%)			Protein content (%)			
	Sum of	F-value	p-value	Sum of	F-value	p-value	
	Squares			Squares			
Model	21.16	6.34	0.0007	236.19	1.57	0.20	
A-Power (W)	10.19	42.79	< 0.0001	7.50	0.70	0.42	
B-	0.01	0.02	0.88	82.32	7.67	0.02	
Solute/water(g/ml)							
C-Sonication time	1.12	4.69	0.04	1.42	0.13	0.72	
(min)							
D-Total volume	4.11	17.24	0.0009	2.25	0.21	0.65	
(ml)							
AB	0.69	2.93	0.11	25.35	2.36	0.15	
AC	0.00	0.00	0.96	0.66	0.06	0.81	
AD	0.03	0.13	0.72	4.65	0.43	0.52	
BC	1.07	4.50	0.05	1.56	0.15	0.71	
BD	0.64	2.68	0.12	0.89	0.08	0.78	
CD	0.11	0.47	0.50	5.06	0.47	0.50	
A ²	1.67	6.99	0.02	19.35	1.80	0.20	
B ²	0.70	2.93	0.11	53.63	4.99	0.04	
C ²	0.06	0.27	0.61	60.05	5.60	0.03	
D ²	0.36	1.49	0.24	22.51	2.10	0.17	
Residual	3.34			150.18			
Lack of Fit	3.02	3.81	0.11	144.85	10.87	0.02	

Pure Error	0.32		5.33	
Cor Total	24.48		386.36	

significant at a 5 % level of significance.

194

195 **Perturbation plot**

196 As the focal point of the experimental design, Fig. 3 illustrates the combined influence of 197 factors on the yield and protein content of faba bean protein extraction. By changing one 198 variable while keeping the other variables constant, the extraction yield perturbation plot was generated. With the exception of factor B (solute/solvent ratio), it was shown that power, 199 200 sonication duration, and total volume significantly impacted extraction yield. This was indicated by the relatively flat line of factor B in Fig 3.A indicating lower influence on 201 extraction yield. Power, or Factor A, has the steepest curve, indicating its exceptional 202 significance in the extraction process. Followed by total volume D, with also a positive effect 203 204 on extraction yield. In contrast to factors A and D, factor C (sonication duration) showed a comparatively flat trend, yet it significantly affected the extraction yield. Perturbation results 205 showed increasing total volume was not suitable for maximizing extraction yield. In the case 206 of protein content (%), the one factor that was observed to be significant was the ratio of solute 207 208 to solvent ratio. Both Fig. 3.A and B, show that the solid-to-solvent ratio had a significant impact on the protein content and extraction yield and protein content. This behavior may be 209 attributed to an enhanced driving force for the mass transfer of proteins, which promotes the 210 diffusion of the solvent into cell compartments and facilitates protein release from the solute 211 (Bedin et al., 2020). 212

213



219

Fig 3. Perturbation plot for faba bean protein (A) extraction yield and (B) Protein content (A:
Power, B: Solid/solvent ratio, C: Sonication time, D: Total volume).

Effect of independent variables on extraction yield (%) and protein content (%)

224 UAE was more effective in the current investigation at extracting proteins from faba beans.

Given its excellent scalability, Suchintita Das et al., (2022b) claimed that the UAE represent a

very promising approach in this regard. Through the combined effects of cavitation, agitation,

and thermology, UAE demonstrates greater extraction efficiency from plant sources (Navaf et

- al., 2023). Numerous research studies support UAE's effective deployment to extract proteins
- from plant sources such as those from mustard meal (Jahan et al., 2022), alfafa flour (Hadidi
- et al., 2020), and moringa oleifera seeds (Fatima et al., 2023).

Using Design-Expert software, the three-dimensional (3D) response surface plot was 231 constructed. The 3D plots allow the possibility to visualize the interactions between the 232 experimental factors and the response between two test factors (Guo et al., 2018). Every 233 response surface displays the function of two variables, while the third variable remains 234 constant. In the event where the response surface graph was curved, the quadratic term was 235 236 significant on the plot (Fatima et al., 2023). Extraction of proteins was done using a constant Alkaline solubilization of pH 11 and isoelectric precipitation of pH 4 based on previous studies 237 (Badjona et al., 2024b; Jeganathan et al., 2023). Fig.4. A-F illustrates the 3-D plots interactions 238 for extraction yield. The values of extraction yield by solute to solvent ratio and power while 239 240 maintaining total volume and sonication time constant are represented in Fig.4. A. Increasing the solute and solvent ratio and higher ultrasonic power showed an increasing extraction yield. 241 High solute/solvent ratio enhances the contact between faba bean flour and the solvent, 242 243 resulting in an increase of protein in the dispersion.

At high solvent to solute ratios, there was a greater rate of extraction, which may indicate 244 improved interaction with the sample environment through increased sonication power, 245 246 allowing mass transfer and cell wall penetration. Further increasing sonication power results in a decrease in extraction yield due to protein gradient reduction (Rashid et al., 2022). This can 247 also be observed in the quadratic effects where both solute-to-solvent ratio and power had a 248 significant impact on the extraction yield. Therefore, 0.06 (1:15 g/mL) was selected as the best 249 250 flour-to-water ratio. As shown in Fig.4.B, the relationship between sonication time and sonication power showed that increasing sonication time increased the yield of protein 251 extraction (not significant) with minimal effect compared to ultrasonic power. High ultrasound 252 power and relatively longer sonication time resulted in ultrasonic cavitation which was 253 conducive to the diffusion of protein from the cell to the solvent (Liu et al., 2019a). The results 254 of the current investigation supported the claims made by Brahmi et al., (2022), which indicated 255

that the extraction rate of biological compounds increase in 30 minutes before subsequentreduction in yield.

Fig.4.C showed that increasing sonication time and solute-to-solvent ratio led to an increase in 258 extraction yield with a significant effect observed for solute/solvent ratio. In general, maximal 259 extraction yield was found higher between 30 - 60 min. Similar research has shown that 260 extending the extraction period beyond 60 min did not increase the protein extraction yield 261 (Eromosele et al., 2008; Qiu et al., 2023). On the other hand, Fig.4.D shows the effect of total 262 solution volume and ultrasonic power on extraction yield. A higher total extraction volume was 263 found to be less desirable while a higher power was suitable to increase extraction yield. Total 264 extraction volume had negative effect, meaning that the extraction yield of faba bean protein 265 was more suitable at low extraction volume. 266

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Fig.4. Response surface plots for the interaction between sonication power, sonication time,
solute-to-solvent ratio, and extraction volume on extraction yield (%). (A) shows the interaction
between solute/solvent ratio and Power; (B) sonication time vs Power; (C) sonication time vs
solute/water ratio; (D) Total volume vs Power; (E) Total volume vs sonication time (F) Total
volume VS solute/solvent ratio on extraction yield.



Fig.5. 3D master plot of combined effect of solute to solvent ratio(g/mL) against Wmin/mL

294 (Power*time/Total volume). Labels (x,y) represent x(solute/solvent ratio: g/mL); y

295 (power*Total volume : P*t/TV).

Aside from extraction yield that is mostly used to characterize extraction efficiency, protein content also represents a major variable for quantifying effectiveness of an optimization process. Depending on the process conditions, the protein content in the current study ranged from 79 to 92%. In the case of protein content, somewhat similar observations were observed as shown in **Fig.6. A-F**. Generally, higher protein content is obtained with a moderate volume of sonicating solution, sonication power and sonication time, and a higher solute-to-solvent ratio of 0.06 (1:15 g/mL). As shown in **Fig.6. A**, there was no significant increase in protein

303	content with longer sonoprocessing times; nonetheless, the maximum protein content was
304	reached at ~30 min as opposed to 60 min. The prolonged treatment may have caused a
305	temperature rise, which in turn reduced surface tension and viscosity and increased vapour
306	pressure, hence minimizing sonication impact (Suchintita Das et al., 2022b). In contrast, the
307	protein content increased with a high solid/solvent ratio as shown in Fig.6. B. A high solute-
308	to-solvent ratio creates a high gradient in protein concentration in and out the cell matrices,
309	thereby improving protein content (Fatima et al., 2023). Thus, an optimum value of 0.06 (1:15
310	g/mL) was found to be the best. Protein matrix, extraction process, source of material and other
311	factors affects the choice of solute/solvent ratio (Chemat et al., 2017). Other studies have shown
312	an improvement in protein content after sonication, for instance soybean protein (Ding et al.,
313	2021), yam bean protein (Eromosele et al., 2008) and wampee protein (Liu et al., 2019b).
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Fig 6. Response surface plots for the interaction between sonication power, sonication time,
solute-to-solvent ratio, and extraction volume on protein content (%). (A) shows the interaction
between sonication time vs Power; (B) Solute/water ratio vs Power; (C) Total volume vs Power;
(D) Total volume vs sonication time; (E) Total volume vs solute/water ratio; (F) sonication time
vs solute/water ratio on protein content %.

The plot in Fig.7. shows values of extraction yield (%) and protein content (%) variables to 341 solute/solvent ratio and Power(W) variables. These contour diagrams were used to analyze the 342 relationship between the three variables. One dependent variable is displayed on the z-axis, 343 while two independent variables are displayed on the x and y axes. Contour plots are a useful 344 tool for determining which combinations yield favorable results. With the desirability 345 technique, responses are assigned a numerical value between 0 and 1, and variable settings are 346 selected to increase the score for the optimisation of aggregate responses (Ares, 2014). A 347 348 composite desirability of 0.6 - 0.8 is considered a satisfactory value according to Jarpa-Parra et al., 2014), hence the result of 0.83 in this present study is suitable. Verification tests were 349 carried out in these conditions in order to assess and validate the reliability of the results. 350

353 Desirability Extraction yield (%) 0.25 0.25 0.4 354 0.212 0.212 0.6 B: Solute/water (S/W) B: Solute/water (S/W) 0.174 0.174 17 18 355 0.136 0.136 0.8 356 0.09 0.098 Desirability 0 357 128 102 128 A: Pow (W) A: Power (W) Protein content % 358 0.25 86 0.212 359 B: Solute/water (S/W) 0.17 360 90 0.13 361 0.09 ediction 89.7613 362 86 0.06 A: Power (W)

Fig 7. Contour plot on Desirability (Solute/solvent ratio vs Power).

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365 Simultaneous validation and optimization of the isolation process

366 Simultaneous optimization of extraction yield and protein content of the ultrasound-assisted 367 alkaline isoelectric precipitation on faba bean protein isolate was carried out experimentally to 368 compare to predicted results. The suitability of the generated model was validated and tested 369 based on the optimal conditions recommended to give maximal responses.

The following conditions: Power 123 W, solute to solvent ratio 0.06 (1:15 g/mL), sonication

time 41 min, and total volume 623 mL were predicted to give a maximal yield of 18. $71 \pm 1 \%$

and protein content of $89.76 \pm 1\%$. In most ultrasound assisted extraction of proteins from plant 372 materials, the crucial limit range between 20 and 60 min (Suchintita Das et al., 2022b). This 373 duration may vary based on ultrasound equipment and other extraction conditions applied. 374 These fixed conditions: Power 123 W, solute to solvent ratio 0.06 (1:15 g/mL), sonication time 375 41 min, and total volume 623 mL after experimental confirmation showed an extraction yield 376 377 of 19. 75 \pm 0.87 % and protein content of 92.87 \pm 0.53 % (n=3). Thus, the quadratic model used in this study was useful to obtain optimal conditions necessary to produce protein isolate 378 from faba beans flour. A control sample under similar conditions without ultrasound showed 379 an extraction yield of 16.41 ± 0.02 % and protein content of 89. 88 ± 0.40 % (n=3). Using 380 381 alkaline extraction of faba bean isolates, a protein purity of roughly 80 – 90 % has been attained by Krause et al., (2023). Optimised ultrasound-assisted alkaline extraction in the present study 382 resulted in an improvement in protein purity which could be attributed to ultrasound effects 383 384 (Kingwascharapong et al., 2021) as well as the optimised process conditions.

385

386 Conclusion

387 The market for faba bean protein is predicted to rise sharply as a result of consumers' rising interest in eco-friendly and sustainable products. For the food and other industries, faba beans 388 can provide a reliable source of alternative protein. This work investigated the production of 389 390 faba bean protein isolates using ultrasound-assisted alkaline isoelectric precipitation. A Box-391 Behnken RSM was used to optimize extraction yield and protein content simultaneously. The 392 obtained findings indicated that the solid-to-solvent ratio, sonication time, Power (W), and total extraction volume, affected the measured responses. The maximum extraction yield (19.75 %) 393 and protein content (92.87 %) were reached following optimized conditions: Power of 123 W, 394 395 solute/solvent ratio of 0.06 (1:15 g/mL), sonication time of 41 min, and total volume of 623

396 mL. Additional control protein isolates without ultrasound application generated an extraction 397 yield and protein content of 16.41 % and 89.99 % respectively. This work demonstrates the 398 excellent potential of utilizing the DoE-based approach for the optimization of protein 399 extraction from faba beans, and a BBD model with specified parameters was found to be the 400 most effective for a quicker and more efficient protein recovery with a superior extraction yield 401 and protein purity. The green protein extraction process presented in this study might be further 402 explored for possible industrial scale-up to understand its limitations and cost implications.

403

404 Declaration of competing interest

The authors declare that they have no known competing financial interests or personal

406 relationships that could have appeared to influence the work reported in this paper.

407 Authorship contribution statement

Abraham Badjona: Investigation, Writing – review & editing, Data curation, Formal analysis,
Methodology, Writing – original draft. Robert Bradshaw: Conceptualization, Methodology,
Supervision, Writing – original draft, Writing – review & editing. Caroline Millman:
Supervision, Writing – review & editing. Martin Howarth: Conceptualization, Supervision,
Writing – review & editing. Bipro Dubey: Conceptualization, Data curation, Methodology,
Supervision, Writing – original draft, Writing – review & editing.

414 Data Availability Statement

415 The data generated during the current study are available upon reasonable request.

416

418 Rights Retention Statement

- 419 For the purpose of open access, the author has applied a Creative Commons Attribution
- 420 (CCBY) licence to any Author Accepted Manuscript version of this paper arising from this
- 421 submission.
- 422

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