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Supporting Information

Carbon Matrix with Atomic Dispersion of Binary Cobalt/Iron-N Sites as Efficient Peroxymonosulfate Activator for Organic Pollutants Oxidation

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S1. Chemicals

$\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$, $\text{Co}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$, 1,4-benzenedicarboxylic acid (1,4-BDC), N, N-dimethylformamide (DMF), melamine, methanol (MeOH), tert-Butyl Alcohol (TBA), p-benzoquinone, 1,10-phenanthroline and furfuryl alcohol were purchased from Siyaku Chemical Reagent Co., Ltd., Japan. All reagents used were analytical grade reagents.

S2. Characterization

X-ray diffraction (XRD) patterns were obtained from an X-ray diffractometer with Cu $K\alpha$ radiation, then were applied to evaluate the crystal structure of the samples. The morphology and composition of catalysts were analyzed by scanning electron microscopy and transmission electron microscopy (SEM/TEM, JEM-3200FS) and energy-dispersive X-ray spectroscopy (EDX). The X-ray absorption fine structure spectra were measured on the 1W1B station in Beijing Synchrotron Radiation Facility (BSRF). Data were collected through a fixed-exit double-crystal Si (111) monochromator. The obtained data were analyzed by Athena and Artemis. Surface electronic states were recorded by X-ray photoelectron spectroscopy (XPS, VG MultiLab 2000). The N_2 adsorption-desorption measurements were analyzed by the nitrogen adsorption apparatus (ASAP 2020, USA). The iron and cobalt concentration were measured using inductively coupled plasma optical emission spectroscopy (ICP-OES). The total organic carbon (TOC) was analyzed using a multi N/C 3100 analyzer. ^{57}Fe Mössbauer spectra of Fe-MOF and $\text{FeN}_x\text{-C}$ catalysts were obtained using ^{57}Co (Rh) γ -ray radioactive source maintained at room temperature (298 K). EPR spectra were recorded using a Bruker ESR A300-10/12 spectrometer at room temperature. The open-circuit voltage, linear sweep voltammetry (LSV) and electrochemical impedance spectroscopy (EIS) were performed on a CHI 660D electrochemical workstation with a standard three-electrode electrochemical cell (Pt electrode, FTO glass and saturated calomel electrode). Firstly, the

homogeneous catalyst ink was prepared: 5 mg catalyst was dissolved in 250 μL DI and 20 μL Nafion reagent and then ultrasonicated for 30 min. Afterwards, the mixture was dropped onto the FTO glass surface (1 x 1 cm) and dried in ambient environment. Specifically, Nyquist plots were measured under frequency from 10^5 to 10^{-2} Hz at a stable initial voltage. LSV measurement was conducted at potential range of 0V-1V vs Ag/AgCl with a scan rate of 50 mV. Open-circuit voltage was performed in a standard three electrode electrochemical cell. After waiting for the open circuit voltage to stabilize, PMS and BPA were added at an interval of 200 seconds. As for the turnover frequency (TOF) value calculation, the ratio of the molar amount of substrate converted to the molar amount of catalyst used in a reaction in unit time, as shown below:

$$\text{TOF} = \frac{\text{moles of degraded substrate}}{\text{mole of active sites} \times \text{reaction time}}$$

S3. Density functional theory (DFT) calculation

Density functional theory calculations were performed using Vienna Ab Initio Package (VASP) within the generalized gradient approximation (GGA) using the PBE formulation. The projected augmented wave (PAW) potentials to describe the ionic cores and take valence electrons into account using a plane wave basis set with a kinetic energy cutoff of 450 eV. Partial occupancies of the Kohn–Sham orbitals were allowed using the Gaussian smearing method and a width of 0.05 eV. The electronic energy was considered self-consistent when the energy change was smaller than 10^{-5} eV. A geometry optimization was considered convergent when the force change was smaller than 0.03 eV/Å. Finally, the adsorption energies (E_{ads}) are calculated as $E_{\text{ads}} = E_{\text{ad/sub}} - E_{\text{ad}} - E_{\text{sub}}$, where $E_{\text{ad/sub}}$, E_{ad} and E_{sub} are the optimized adsorbate/substrate system, the adsorbate in the structure and the clean substrate, respectively.

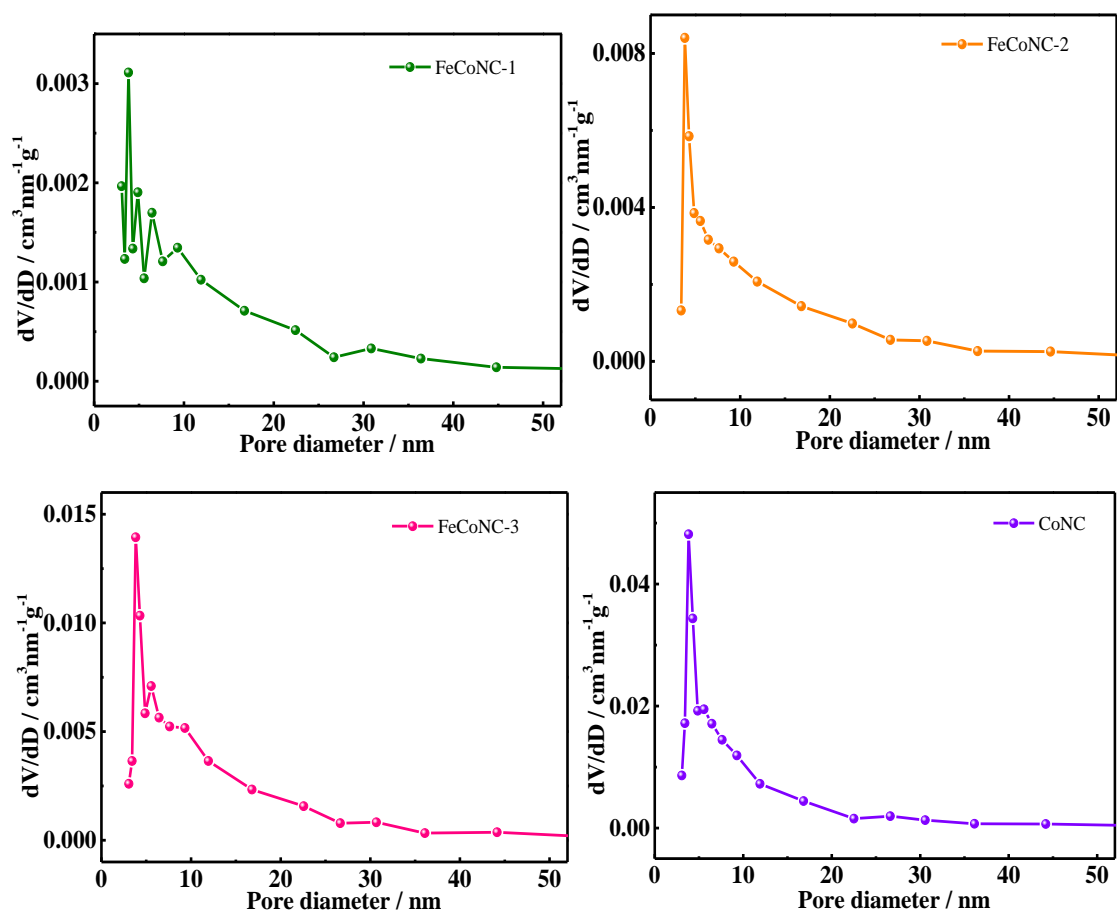


Figure S1. N_2 adsorption-desorption isotherm and pore size distribution of as-synthesized catalysts

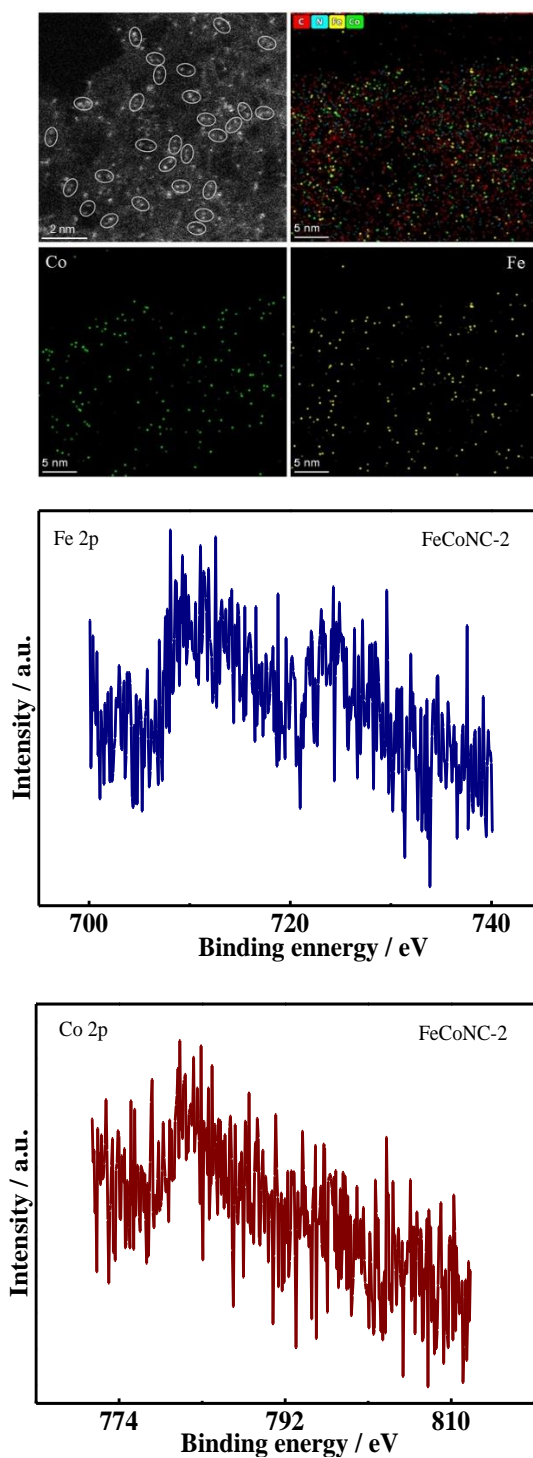


Figure S2. HAADF-STEM image and EDS-mapping images; High resolution XPS spectra of Fe 2p and Co 2P in FeCoNC-2 catalyst

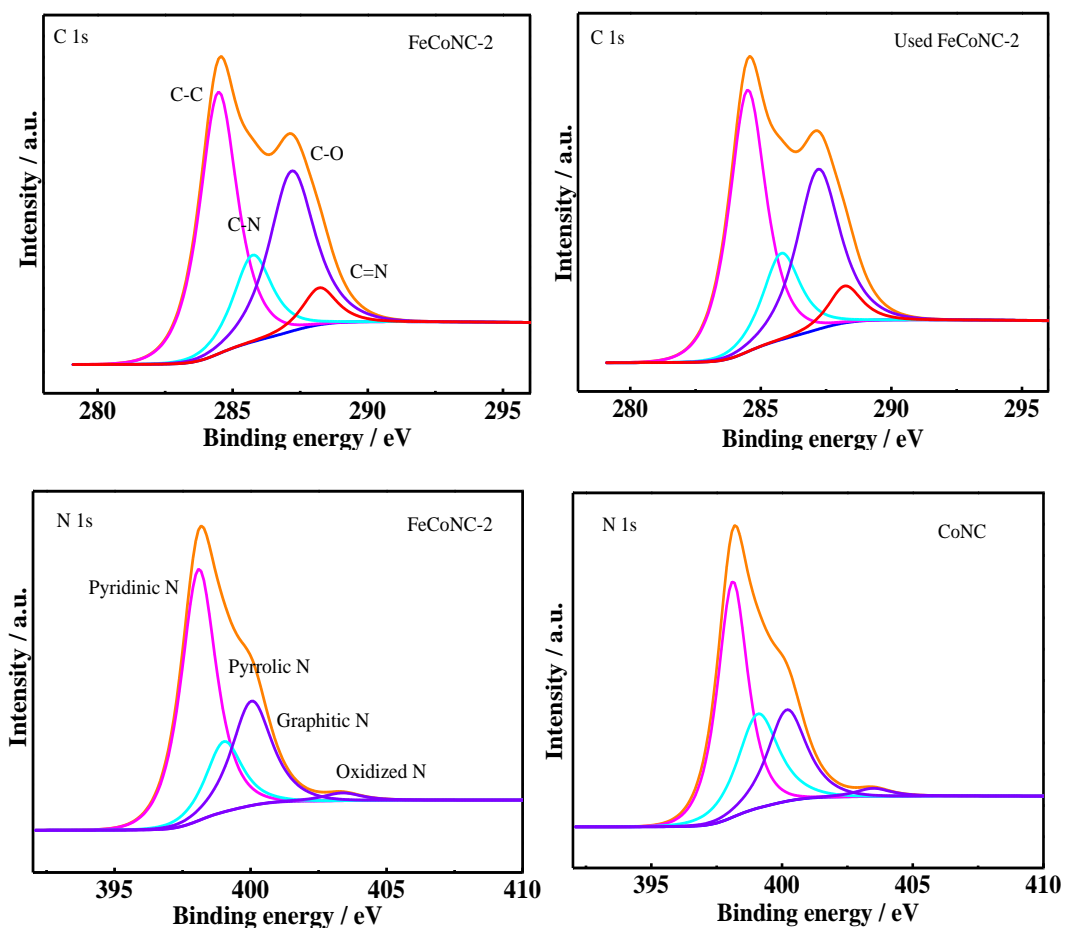


Figure S3. High resolution C 1s XPS spectra of fresh and used FeCoNC-2 catalysts; N 1s XPS spectra of FeCoNC-2 and CoNC catalysts

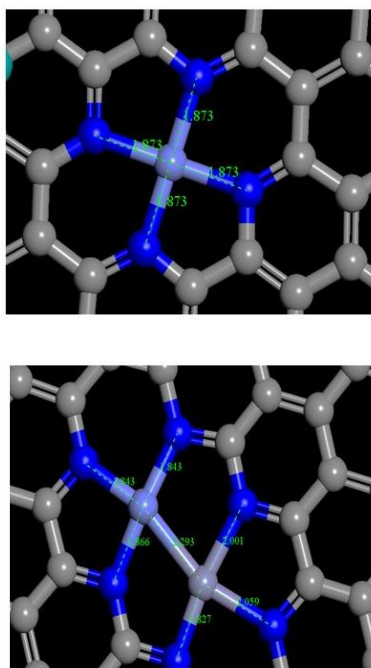


Figure S4. Bond length between Fe, Co and N atoms in CoNC (above) and FeCoNC (below) catalysts

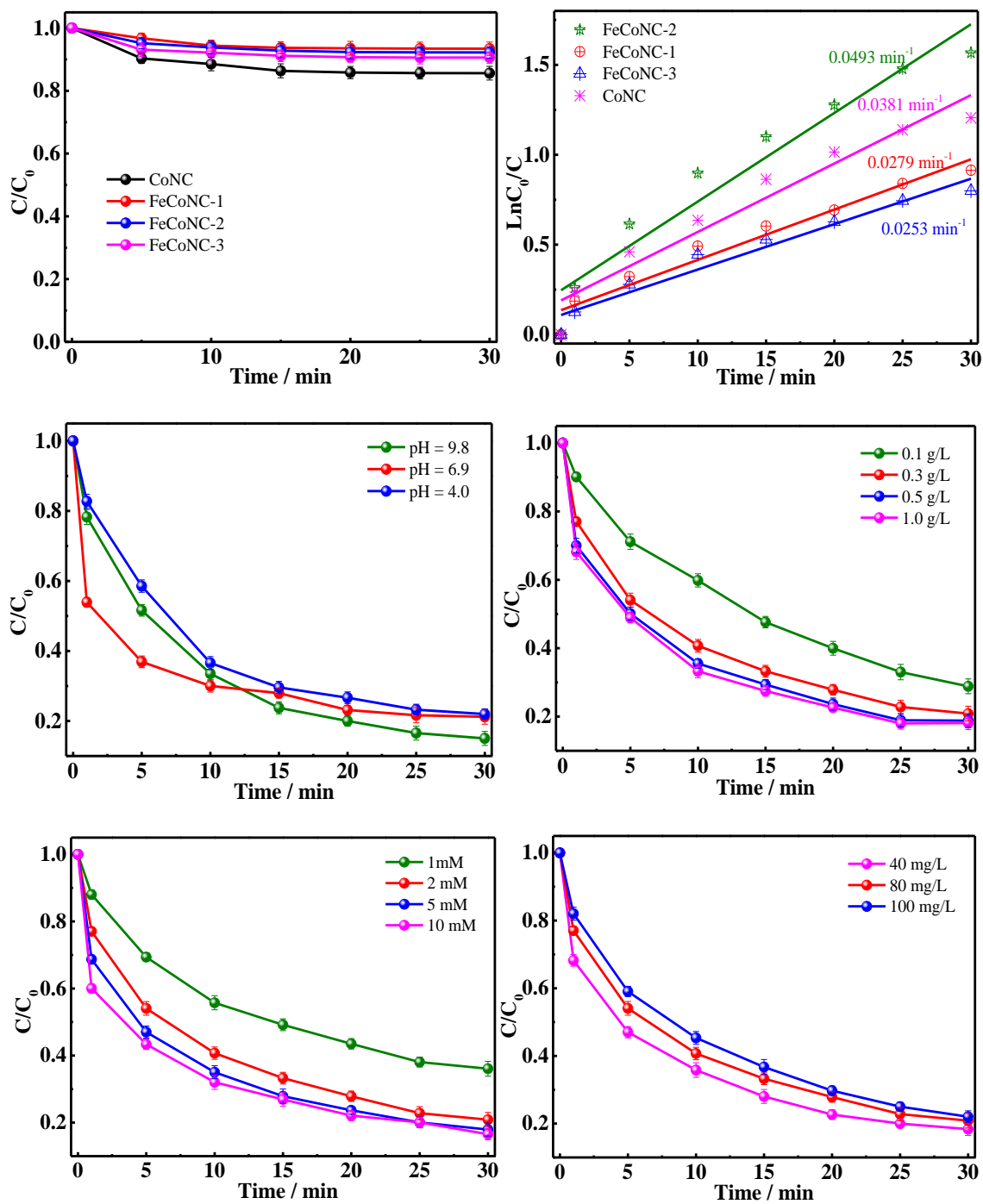


Figure S5. (a) The adsorption ability towards TC via synthesized catalysts; (b) Kinetic curve of TC degradation via synthesized catalysts; TC degradation under different parameters: (c) initial pH value; (d) catalyst dosage; (e) PMS concentration and (f) TC concentration

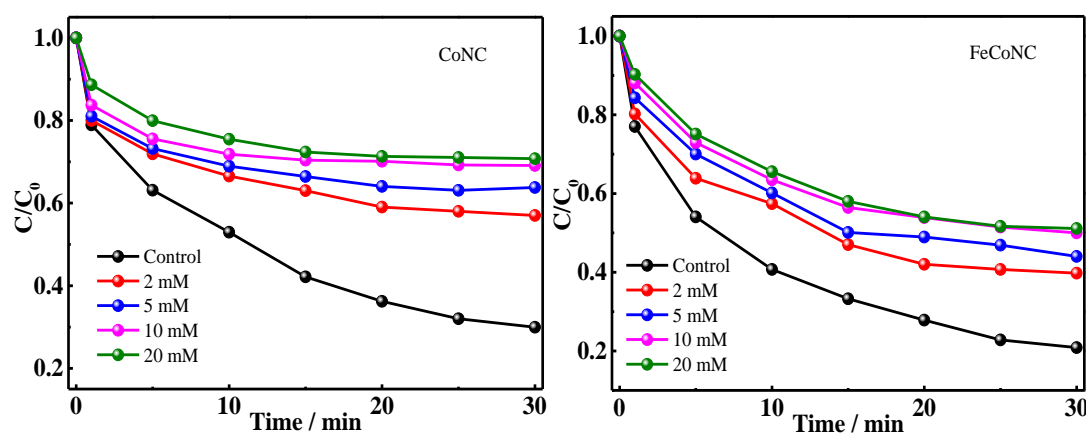


Figure S6. Effect of FFA concentration on TC removal rate in CoNC/PMS and FeCoNC/PMS systems

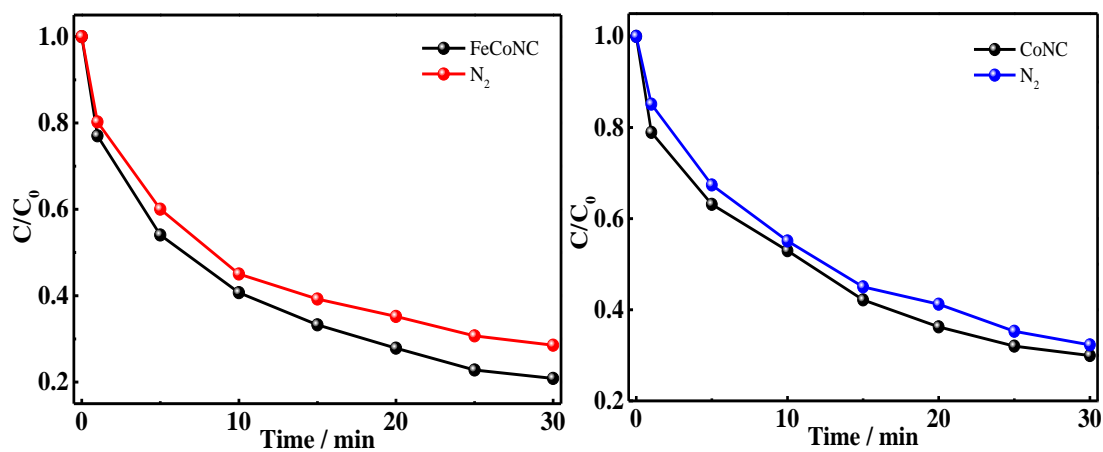


Figure S7. Degradation of TC in the presence or absence of N_2 in FeCoNC and CoNC/PMS system

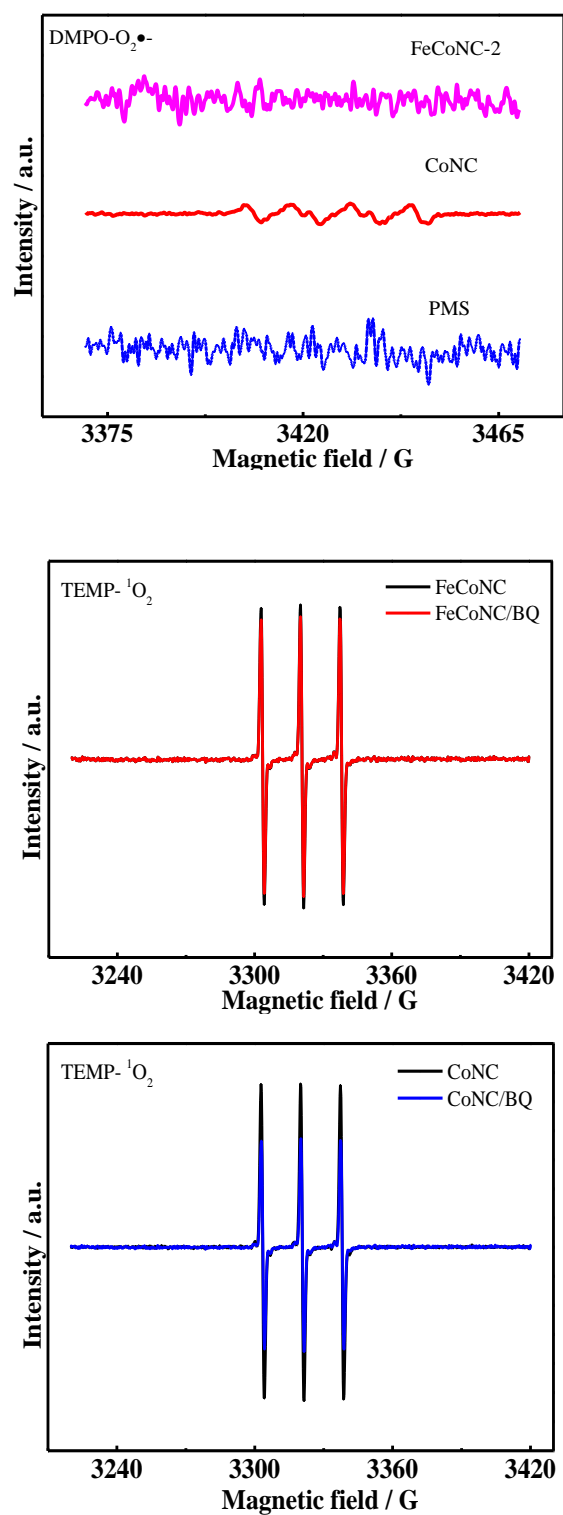


Figure S8. EPR spectra of $^1\text{O}_2$ generated by FeCoNC and CoNC in the presence of BQ scavenger

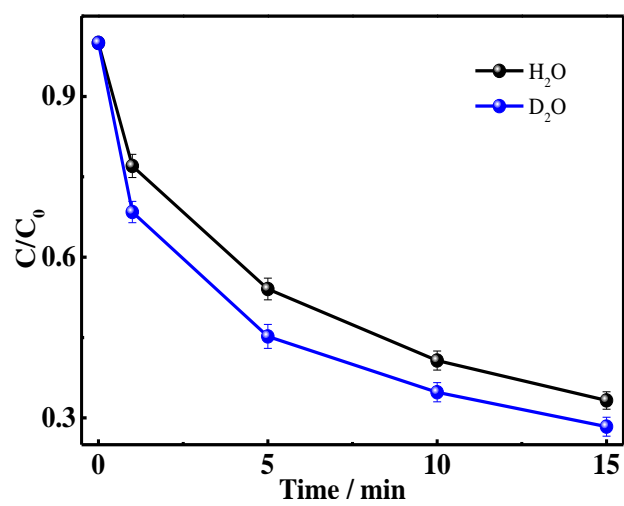


Figure S9. TC degradation efficiency in the FeCoNC/PMS system in the presence of H_2O or D_2O

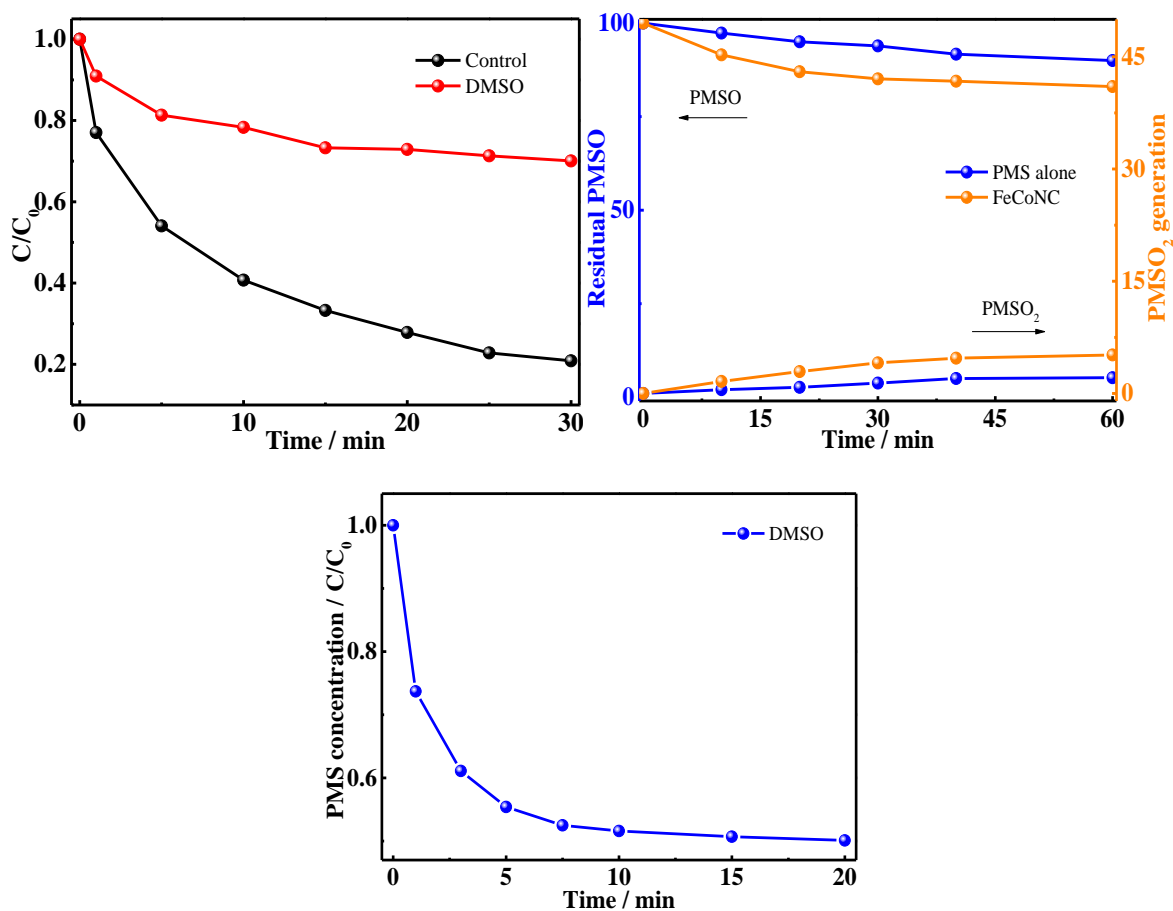


Figure S10. (a) Effect of DMSO scavenger on TC degradation in FeCoNC/PMS system; (b) PMSO consumption and PMSO₂ generation in PMS alone and FeCoNC systems; (c) Consumption of PMS by DMSO scavenger

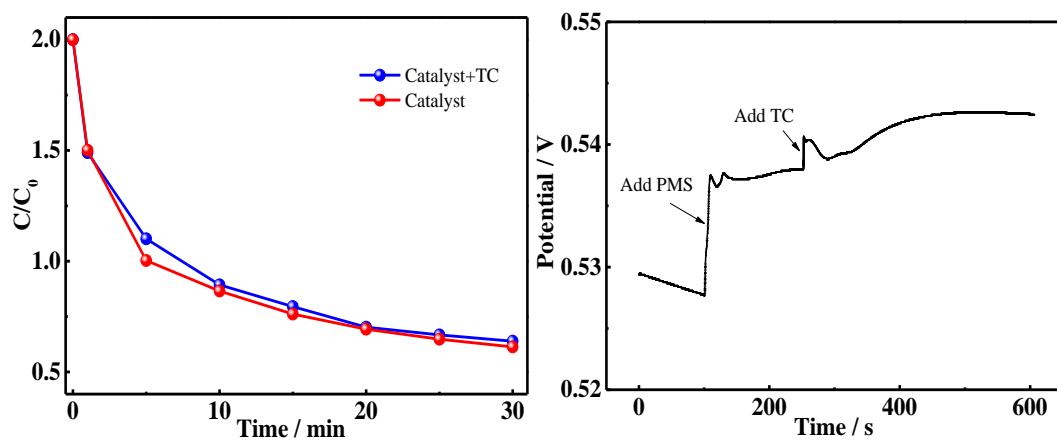


Figure S11 (a) FeCoNC-initiated PMS decomposition; (b) Chronopotentiometry curve with adding PMS and TC solutions

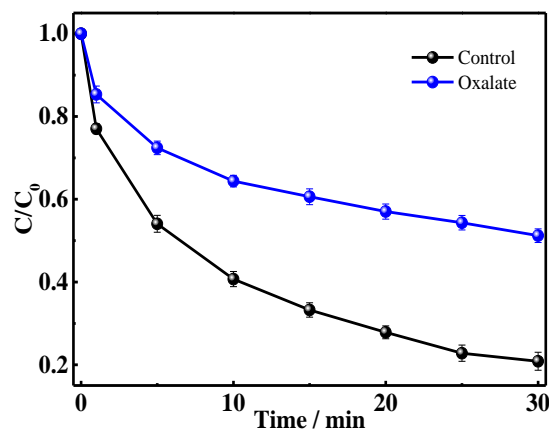
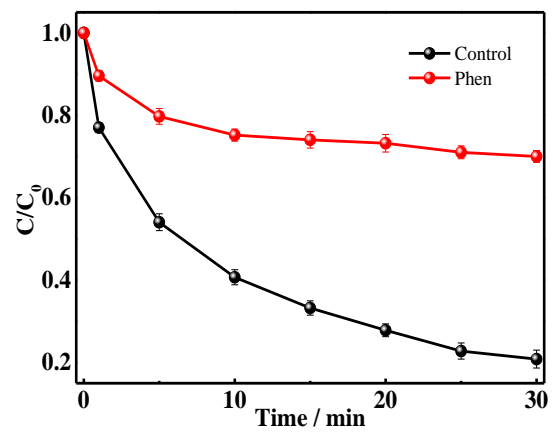


Figure S12. Influence of phenanthroline (Phen) and Oxalate on TC degradation by FeCoNC-2 catalyst

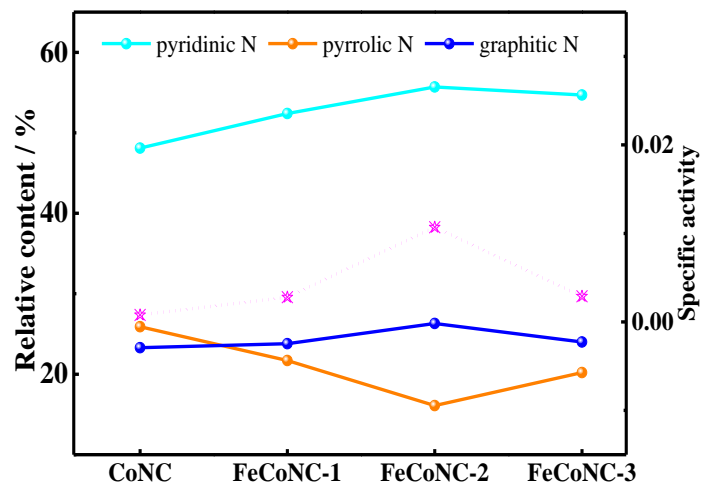


Figure S13. Correlation ship between specific catalytic activity and relative content of N species

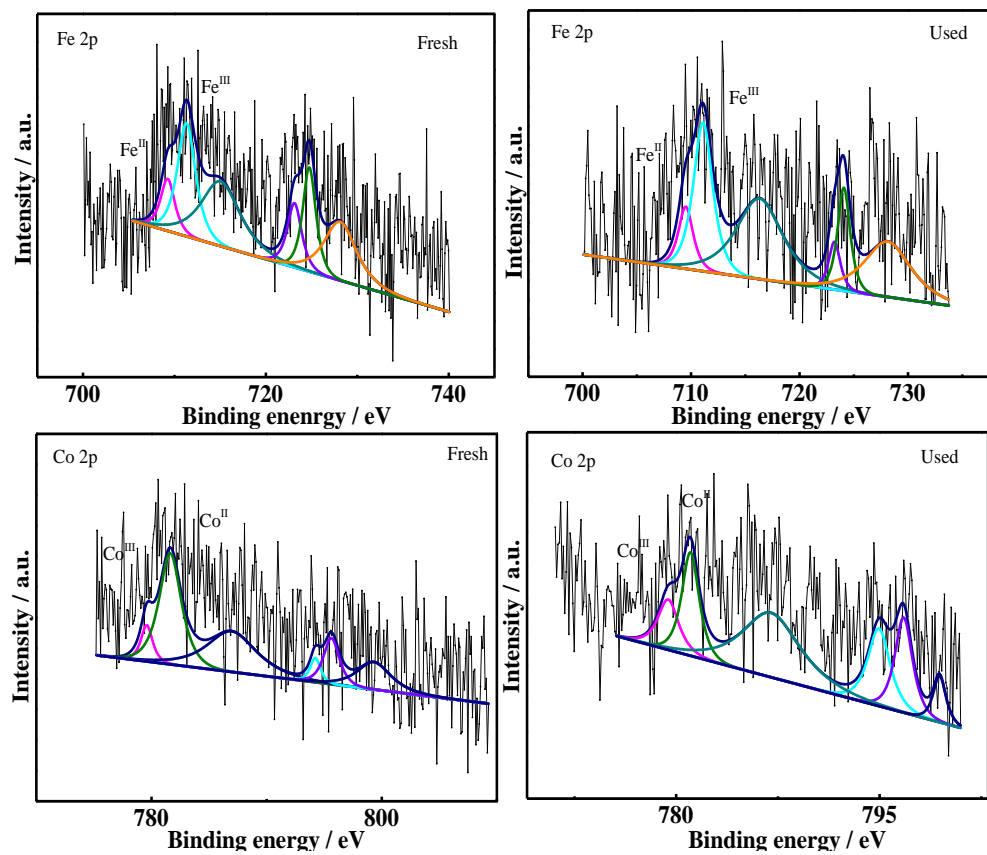


Figure S14. High resolution Fe 2p XPS spectra and Co 2p spectra of FeCoNC-2 catalyst before and after reaction

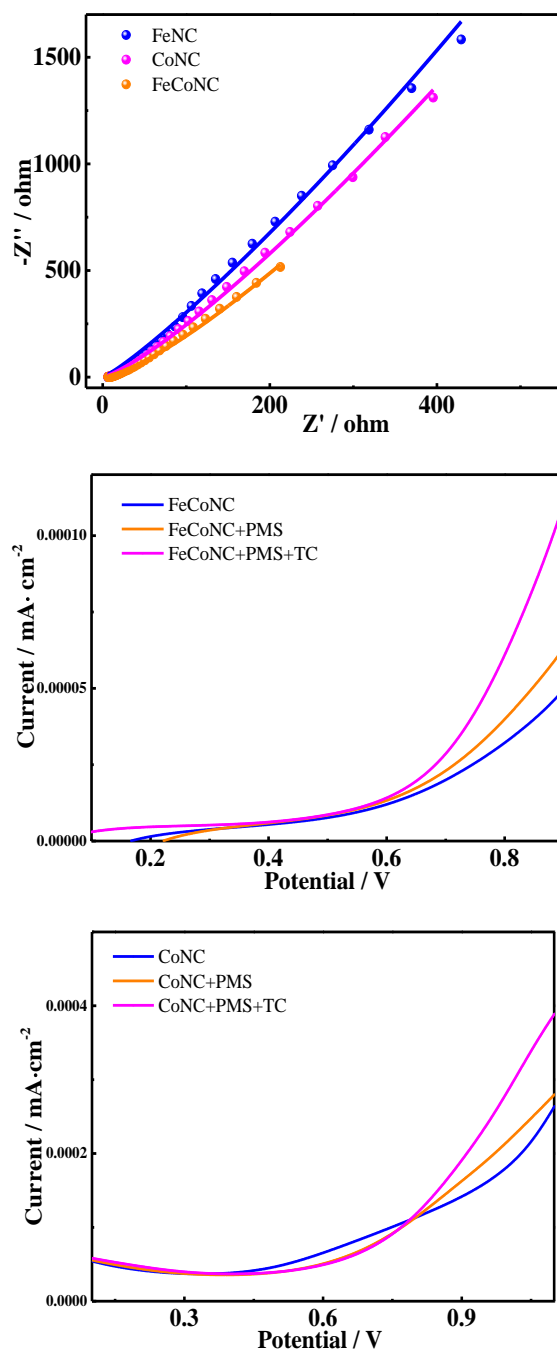


Figure S15. (a) EIS Nyquist plots; (b-c) Linear sweep voltammetry (LSV) curves in different systems

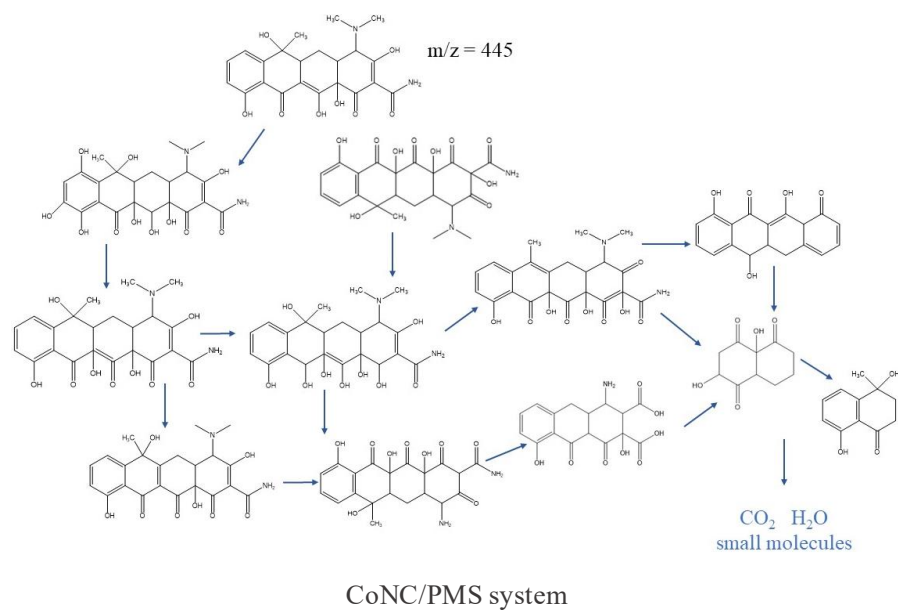


Figure S16. The possible degradation pathways of TC in CoNC/PMS system

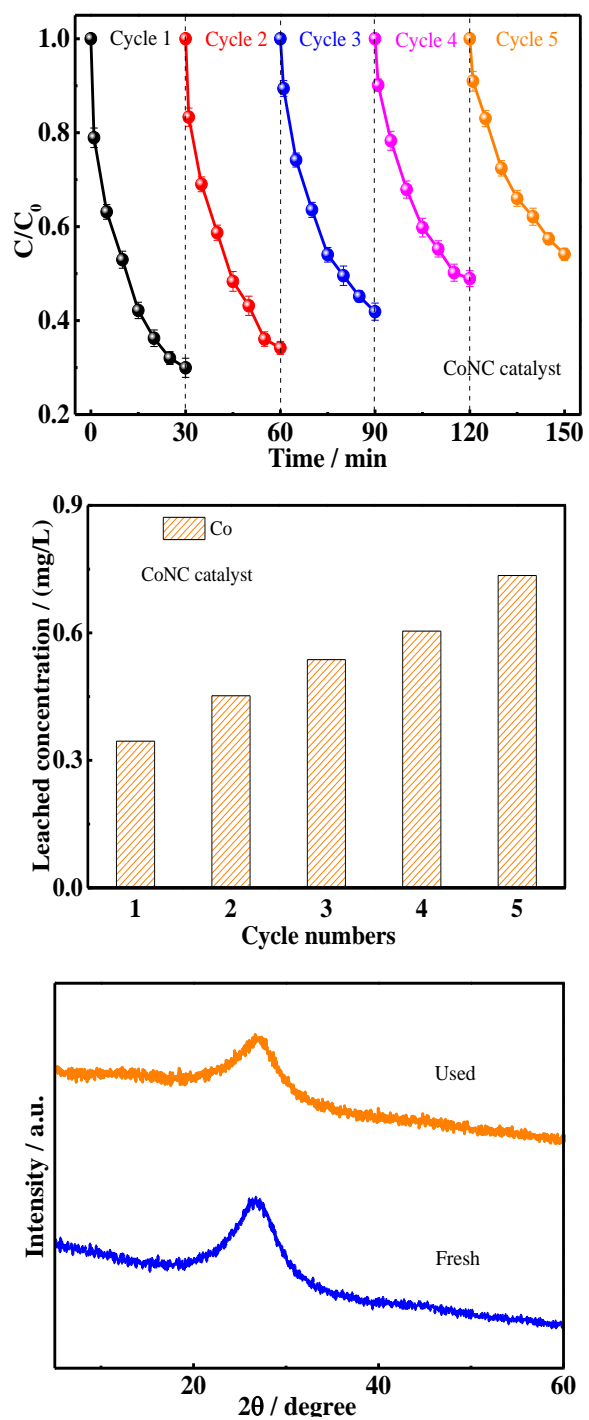


Figure S17. (a) The reusability test of CoNC for TC degradation; (e) Leached metal Co concentration after each cyclic experiment; (c) XRD pattern of fresh and used FeCoNC-2 sample

Table S1. Structural parameters of BET surface area, pore volume and pore size

Catalyst	BET Surface area (m ² /g)	Pore volume (cm ³ /g)	Average pore size (nm)
CoNC	116.81	0.238	3.824
FeCoNC-1	29.45	0.060	3.820
FeCoNC-2	15.36	0.032	3.823
FeCoNC-3	43.24	0.100	3.826

Table S2. Normalized k value for TC degradation by as-prepared catalysts

Catalyst	k value min^{-1}	Normalized k value $\text{L min}^{-1} \text{m}^{-2}$	Turnover frequency (TOF) value min^{-1}
CoNC	0.0381	0.0010	0.042
FeCoNC-2	0.0493	0.0107	0.105
FeCoNC-3	0.0253	0.0029	0.063
FeCoNC-1	0.0279	0.0023	0.087

Table S3. Elemental content of FeCoNC catalysts before and after PMS activation by XPS analysis

Catalyst	Fe	Co	N	O	C
CoNC	--	0.47	35.54	9.38	54.61
FeCoNC-2	0.39	0.28	38.07	6.56	54.70
FeCoNC-2 after PMS activation	0.35	0.26	32.25	12.58	54.56

Table S4. EXAFS fitting parameters at the Co K-edge for FeCoNC and references sample

Sample	Shell	CN^a	$R(\text{\AA})^b$	$\sigma^2(\text{\AA}^2)^c$	$\Delta E_0(\text{eV})^d$	R factor
Co foil	Co-Co	12*	2.49±0.01	0.0061±0.0003	7.1±0.4	0.0006
CoPc	Co-N	3.9±0.7	1.93±0.02	0.0049±0.0023	8.8±2.2	0.0132
FeCoNC	Co-N	2.9±0.7	1.91±0.04	0.0067±0.0037	6.4±1.0	0.0175
	Co-Fe	0.9±0.4	2.73±0.01	0.0056±0.0032	7.3±1.8	

^a CN , coordination number; ^b R , distance between absorber and backscatter atoms; ^c σ^2 , Debye-Waller factor to account for both thermal and structural disorders; ^d ΔE_0 , inner potential correction; R factor indicates the goodness of the fit. S_0^2 was fixed to 0.71, according to the experimental EXAFS fit of Co foil by fixing CN as the known crystallographic value. A reasonable range of EXAFS fitting parameters: $0.700 < S_0^2 < 1.000$; $CN > 0$; $\sigma^2 > 0 \text{ \AA}^2$; $|\Delta E_0| < 10 \text{ eV}$; $R \text{ factor} < 0.02$.

Table S4. EXAFS fitting parameters at the Fe K-edge for FeCoNC and references sample

Sample	Shell	CN^a	$R(\text{\AA})^b$	$\sigma^2(\text{\AA}^2)^c$	$\Delta E_0(\text{eV})^d$	R factor
Fe foil	Fe-Fe1	8*	2.47±0.07	0.0047±0.0020	5.7±1.4	0.0015
	Fe-Fe2	6*	2.84±0.09	0.0054±0.0043	3.9±2.2	
FePc	Fe-N	4.2±0.9	1.97±0.02	0.0082±0.0020	7.7±1.8	0.0024
Fe sample	Fe-N	3.1±1.2	2.06±0.02	0.0036±0.0027	8.8±2.1	0.0048
	Fe-Co	1.0±0.5	2.75±0.03	0.0093±0.0018	8.0±2.5	

^a CN , coordination number; ^b R , distance between absorber and backscatter atoms; ^c σ^2 , Debye-Waller factor to account for both thermal and structural disorders; ^d ΔE_0 , inner potential correction; R factor indicates the goodness of the fit. S_0^2 was fixed to 0.72, according to the experimental EXAFS fit of Fe foil by fixing CN as the known crystallographic value. A reasonable range of EXAFS fitting parameters: $0.700 < S_0^2 < 1.000$; $CN > 0$; $\sigma^2 > 0 \text{ \AA}^2$; $|\Delta E_0| < 10 \text{ eV}$; $R \text{ factor} < 0.02$.

Table S5. ^{57}Fe Mössbauer parameters and assignment of the components featured in the deconvoluted

Mössbauer spectra of FeCoNC catalysts

Catalyst	Component	IS/ mms^{-1}	QS/ mms^{-1}	Area/%	Assignment
FeCoNC-1	D1	1.250	3.35	20.5	$\text{Fe}^{\text{II}}\text{N}_x$
	D2	0.437	0.98	79.5	$\text{Fe}^{\text{III}}\text{N}_x$
FeCoNC-2	D1	1.258	3.21	15.1	$\text{Fe}^{\text{II}}\text{N}_x$
	D2	0.401	0.838	84.9	$\text{Fe}^{\text{III}}\text{N}_x$
FeCoNC-3	D1	1.099	3.19	21.2	$\text{Fe}^{\text{II}}\text{N}_x$
	D2	0.409	0.99	78.8	$\text{Fe}^{\text{III}}\text{N}_x$
Used FeCoNC-2	D1	1.255	3.45	10.5	$\text{Fe}^{\text{II}}\text{N}_x$
	D2	0.401	0.92	89.5	$\text{Fe}^{\text{III}}\text{N}_x$

Table S6. Comparison of catalytic reactivity of FeCoNC catalyst with previous reported catalysts during PMS
activation

Catalyst	Catalyst dosage (g L ⁻¹)	TC concentration (mg L ⁻¹)	PMS (mM)	Degradation time (min)	Removal rate (%)	Rate constant (min ⁻¹)	Ref.
CA-900	0.2	10	2.0	90	90	0.0096	1[1]
R-N-Fe	0.5	100	2.0	275	80	--	2[2]
Co-MIL-53(Al)	0.3	30	2.0	120	90	0.0310	3[3]
Co-PPCC	1.0	50	1.0	60	90	--	4[4]
PFSC-900	0.4	20	1.0	120	90	0.0317	5[5]
Rice husk biochar	4.0	20	20	120	90	--	6[6]
FeS ₂	2.0	50	1.0	120	89	0.0099	7[7]
MIL-125(Ti)-NH ₂ -Fe	0.1	20	4.5	40	90	0.0355	8[8]
AC@Fe ₃ O ₄	0.2	30	PS/30	180	80.7	0.0098	9[9]
BC/CN-15	0.2	10	1.0	60	89	0.0351	10[10]
FeCo/N-C	0.3	80	2.0	30	82	0.0493	This work

Reference

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